Table 5

Flashing/Working/Breathing Summit Production Facility Ward County Halcon Operating Co., Inc

Promax Tank Loss Stencil Input										
EPN	Ì	FLARE1	FLARE1							
FIN		TK1-4	TK5-8							
Number of Tanks		4	4							
Tank Contents		Oil	Produced Water							
Size	bbl	400	400							
Tank Color		Beige	Beige							
Location		Houston, TX								
Shell Length	ft	20	20							
Shell Diameter	ft	12	12							
Breather Vent Pressure	psig	0.03	0.03							
Breather Vac Pressure	psig	-0.03	-0.03							
Operating Pressure	psig	0	0							
Avg. Percent Liquid	%	50	50							
Max Percent Liquid	%	90	90							
Net Throughput	bbl/day	2500	4500							
Atmospheric Pressure	psia	14.70	14.7							
Max Liq Surface Temperature	°F	99.50	79.20							
VRU Downtime	%	5.00	5.00							
Flare Control Efficiency	%	98.00	98.00							
Flash Gas Oil Ratio	scf/bbl	1693.10	-							

	Oil Tanks						Produced Water Tanks <sup>1</sup>						
Components	Wt % Flash Losses	Flashing Losses (ton/yr)	Working Losses (ton/yr)	Breathing Losses (ton/yr)	Total Losses (lb/hr)	Total Losses (ton/yr)	W/B Mass Fraction (%)	Flashing Losses (ton/yr)	Working Losses (ton/yr)	Breathing Losses (ton/yr)	Total Losses (lb/hr)	Total Losses (ton/yr)	Mass Fraction (%)
Hydrogen	-	•		, ,	` '-	-	` ' -		` ' -				
Helium	-	-	-		-	-	-	-	-	-	-	-	
Nitrogen	1.03	0.96	-		-	0.96	0.00	0.01	-	-	<0.01	<0.01	0.0
Carbon Dioxide	2.39	2.23		-	-	2.23		0.02	-	-	<0.01	0.02	0.00
Hydrogen Sulfide	0.73	0.68		-	-	0.68		<0.01	-	-	<0.01	<0.01	0.00
Methane	51.00	47.49	0.12	<0.01	0.12	47.62	1.19	0.47	<0.01	<0.01	0.11	0.48	1.19
Ethane	12.87	11.99	1.00	0.05	1.05	13.04	10.11	0.12	0.02	<0.01	0.03	0.14	10.1
Propane	12.98	12.09	1.83	0.09	1.92	14.00		0.12	0.03	<0.01	0.04	0.16	18.5
i-Butane	2.39		0.48	0.02	0.50	2.73		0.02	<0.01	<0.01	<0.01	0.03	4.84
Butane	7.10	6.61	1.89	0.10	1.99	8.60	19.21	0.07	0.04	<0.01	0.02	0.10	19.2°
i-Pentane	2.44	2.27	1.09	0.06	1.15	3.42		0.02	0.02	<0.01	0.01	0.04	11.0
Pentane	2.17	2.02	1.25	0.06	1.32	3.34		0.02	0.02	<0.01	0.01	0.04	12.70
Hexane	1.46	1.36	1.13	0.06	1.19	2.55	11.45	0.01	0.02	<0.01	<0.01	0.04	11.45
Heptane	0.80	0.74	0.71	0.04	0.75	1.49	7.21	<0.01	0.01	<0.01	<0.01	0.02	7.2
Octane	1.42	1.32	0.28	0.01	0.29	1.62		0.01	<0.01	<0.01	<0.01	0.02	2.84
Nonane	1.14	1.06	0.07	<0.01	0.07	1.13	0.67	0.01	<0.01	<0.01	<0.01	0.01	0.67
Benzene	0.00	0.00		1	-	0.00	0.00	0.00	0.00	0.00		0.00	0.00
Ethylbenzene	0.00	0.00		1	-	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
Toluene	0.00	0.00		1	-	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00
m-Xylene	0.00	0.00		1	-	0.00		0.00	0.00	0.00		0.00	0.00
Decanes	0.07	0.07		1	-	0.07	0.18	<0.01	<0.01	<0.01	<0.01	<0.01	0.18
Undecane	-	•	0.02	<0.01	0.02			0.00	<0.01	<0.01	<0.01	<0.01	0.0
C12+	-	-	<0.01	<0.01	<0.01	<0.01	<0.01	0.00	<0.01	<0.01	<0.01	<0.01	<0.0
TOTAL UNCONTROLLED LOSSES1:	•	93.12	9.86	0.51	10.37	103.49	100.00	0.93	0.19	<0.01	0.26	1,12	100.00
OTAL UNCONTROLLED VOC LOSSES:		29.77	8.75	0.45	9.19	38.97	88.70	0.30	0.17	< 0.01	0.11	0.47	88.70

<sup>&</sup>lt;sup>1</sup> Total flashing losses based on Gas-Oil Ratio from site specific analytical data

VOC PTE for all tanks = 3.90 + 0.05 = 3.95 tpy, which is <6tpy per tank; therefore, the tanks are not an affected source under NSPS OOOOa

API RVP